IN THE CLAIMS

- (Original) A process for driving a prime mover, said process comprising
- a) positioning a selective membrane between a liquid and a solution having a higher osmotic potential than the liquid, such that the solution becomes pressurised by the influx of liquid across the membrane,
- b) transferring the pressure generated in the solution to another liquid via a pressure exchange system to drive a prime mover,
 - c) recovering the solution,
- d) separating at least some of the solvent from the solution to form a residual product, and
- e) recycling the separated solvent and/or the residual product of step d) to step a).
- 2. (Original) A process as claimed in claim 1, wherein the prime mover is a rotary prime mover.
- 3. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the solution is an aqueous solution.
- 4. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the solution is solution of a salt selected from sodium chloride, potassium chloride, potassium nitrate, magnesium sulfate, magnesium chloride, sodium sulfate, calcium chloride, sodium carbonate, disodium hydrogenphosphate and potassium alum.

- 5. (Original) A process as claimed in claim 3 wherein the aqueous solution is formed by dissolving ammonia and carbon dioxide in water.
- 6. (Original) A process as claimed in claim 5, which is an aqueous solution of ammonia, carbon dioxide, ammonium carbonate, ammonium bicarbonate and ammonium carbamates.
- 7. (Currently Amended) A process as claimed in any one of the preceding elaims claim 1, wherein the solution has a solute concentration of 1 to 400 weight %.
- 8. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the liquid is selected from the group consisting of freshwater, seawater, brackish water and a waste stream from an industrial or agricultural process.
- 9. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the liquid is or comprises the same solvent as the solvent of the solution.
- 10. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein solvent is removed in step d) by a thermal and/or membrane separation method.
- 11. (Original) A process as claimed in claim 11, wherein the solvent is remove using a method selected from evaporation, distillation and crystallization.
- 12. (Original) A process as claimed in claim 11, wherein the solvent is removed by at least one method selected from multi-stage flash distillation, ulti-effect distillation, mechanical vapour compression and rapid spray desalination.

- 13. (Original) A process as claimed in claim 10, wherein the solvent is removed by at least one method selected from ion-exchange, electrodialysis nanofiltration and osmosis.
- 14. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the energy required to remove solvent in step d) is provided by the wind power, thermal energy of the surrounding environment, solar energy, geothermal energy, energy from a biological process, energy from the combustion of fuel and/or excess heat from power plants and other industrial processes.
- 15. (Currently Amended) A process as claimed in-any one of the preceding claims claim 1, wherein at least some of the solvent recovered in step d) is recycled to a liquid for step a).
- 16. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, which comprises using the pressure generated in the solution to transfer the solution to an elevated location, and using the potential energy of the elevated solution to drive the prime mover.
- 17. (Currently Amended) A process as claimed in-any one of the preceding claims claim 1, wherein the solution from step a) is transferred to an elevated height where the ambient temperature is
 - (i) low enough to crystallize at least some of the solute in the solution, or
- (ii) below the freezing point of the solvent to crystallize the solvent, such that the solution is separated into a portion having a low solute concentration and a portion having a high solute concentration.

PCT/GB2004/003450 Preliminary Amendment 66307-361

- 18. (Original) A process as claimed in claim 18, wherein each of said portions is returned to ground level, such that the potential energy of each of the portions can be used to drive the prime mover.
- 19. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the thermal energy required to separate the solvent from the solution is step d) is provided by the compression and decompression of gas.
- 20. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the selective membrane of step a) has an average pore size of 1 to 60 Angstroms, preferably 12 to 50 Angstroms.
- 21. (Currently Amended) A process as claimed in any one of the preceding claims claim 1, wherein the pressurised solution from step (a) is positioned on one side of a further selective membrane, and a further solution having a higher osmatic potential than the pressurised solution is placed on the other side of the membrane, such that the further solution become pressurized by the influx of liquid across the membrane.

5